

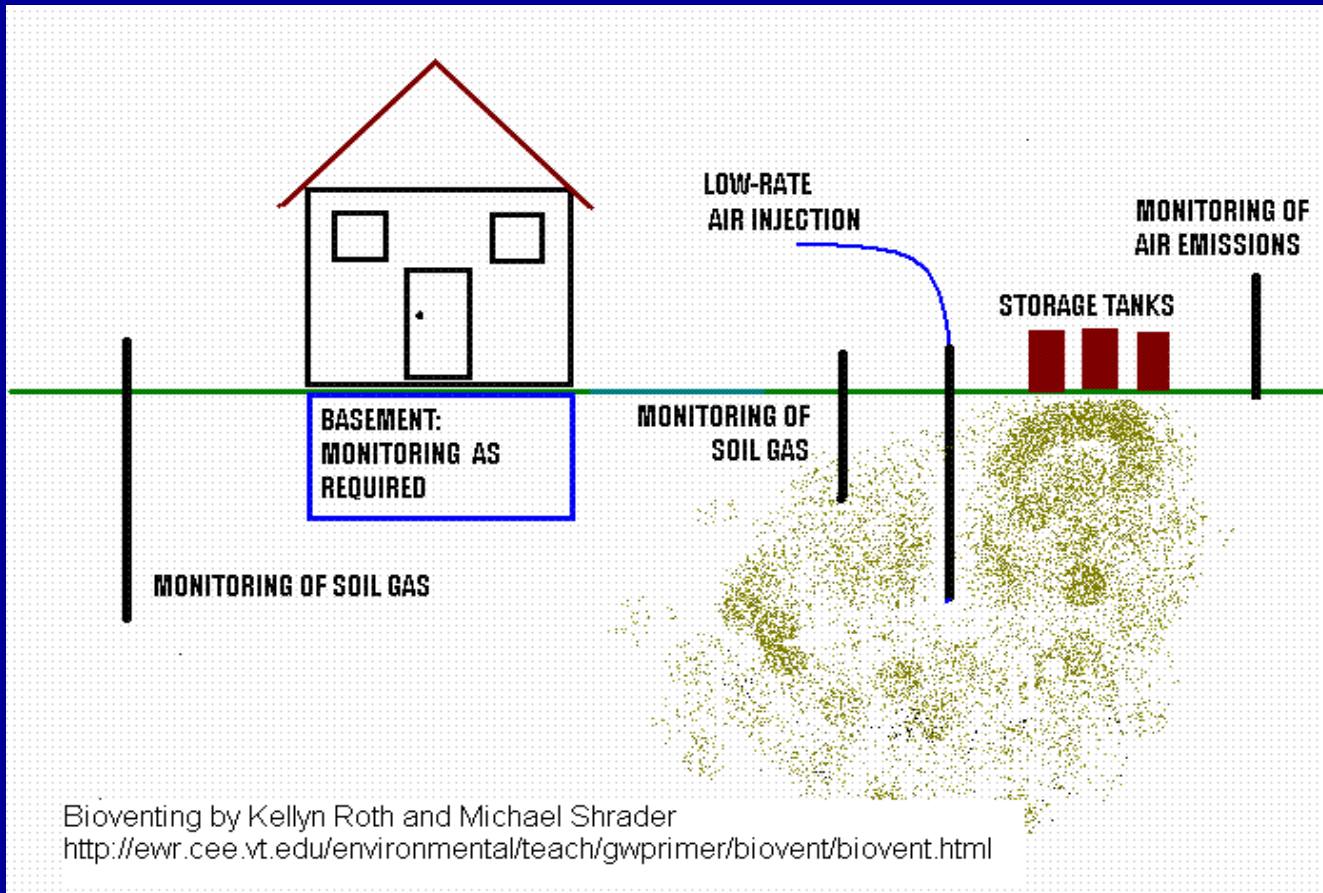
# An Investigation on Remediation of Transformer Oil Contaminated Soil by Chemical Oxidation Using Hydrogen Peroxide

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# Biological remediation technologies



# Biological remediation technologies

## ◆ Process parameters:

- Temperature, type of soils, moisture content
- Soil pH, inorganic nutrients, and Redox potentials
- Electron acceptors

## ◆ Advantages:

- Low cost in investment and simplicity in operation
- Widely accepted by most regulatory agencies
- End products:  $\text{CO}_2$ ,  $\text{CH}_4$ ,  $\text{H}_2\text{O}$ , inorganic salts, and biomass
- Lower MW HC easy to degrade:  $\text{C}_1$ - $\text{C}_{15}$ , R-OH, Ar-OH, R-NH<sub>2</sub>

## ◆ Limitations:

- Relatively long time for treatment
- Dependence on temperature and site conditions
- Limited efficiencies for high molecular weight ( $>\text{C}_{20}$ ) and multichlorinated HC, PAHs, PCBs, and pesticides

# Physical remediation technologies



A soil washing plant

<http://www.art-engineering.com/Projects%20Soil%20Treatment.htm>

# Physical remediation technologies

- ◆ Use contaminant's physical properties to remediate contaminated soils
- ◆ Physical properties include:
  - Density, solubility, liquid viscosity, etc.
  - Vapor pressure, Henry's law constant,  $K_{ow}$ ,
- ◆ Physical removal of contaminants followed by treatments at a plant or off-site
- ◆ Process characteristics
  - Contaminants only go through physical changes
  - Less concerns of the generation of toxic intermediates or products
  - Need to treat the collected contaminants

# Chemical oxidation technologies



A Soil Oxidation Plant

<http://www.art-engineering.com/Projects%20Soil%20Treatment.htm>

# Chemical oxidation technologies

- ◆ Introduction of oxidants into soil to destroy organic contaminants
- ◆ Oxidants:  $\text{Cl}_2\text{O}$ ,  $\text{NaClO}$ ,  $\text{Ca}(\text{ClO})_2$ ,  $\text{KMnO}_4$ ,  $\text{O}_3$  and  $\text{H}_2\text{O}_2$ /Fenton Reagent
- ◆ Intermediates may impact the performance of the oxidant
- ◆ Oxidants are generally non-selective
  - Break C-H, C-C bonds of contaminant organic compounds
  - Oxidation of natural organic matters → substantial increase in total oxidant demand
- ◆ Selection of the appropriate oxidant is dependent upon the:
  - Nature and type of contaminant
  - Level of remediation required
  - Viability of oxidant delivery
  - Type of soil and hydrogeology of the site

# Chemical Oxidation Technologies

## Chemical oxidation potentials

Species	Oxidation power (V)
fluorine	3.03
hydroxyl radical	2.80
atomic oxygen	2.42
ozone	2.07
Hydrogen peroxide	1.78
$\text{MnO}_4^-$	1.60
chlorine	1.36



# Hydrogen Peroxide/Fenton's Reagent

- ◆ Fenton/Fenton-like reaction yielding hydroxyl radicals (OH•) with oxidation power of 2.80V, second only to fluorine, which is the strongest known oxidant
- ◆ Reaction chemistry  $\text{H}_2\text{O}_2 + \text{Fe}^{+2} \rightarrow \text{Fe}^{+3} + \text{OH}^- + \text{HO}\bullet$
- ◆ Easily decompose to  $\text{H}_2\text{O}_{(v)}$  &  $\text{O}_2$
- ◆ Products: organic acids, salts,  $\text{O}_2$ ,  $\text{CO}_2$ , (substantial gas and heat evolution)
- ◆ Low pH favorable (best pH of 2-4) up to near neutral pH
- ◆ OH• radicals are highly active and unstable
- ◆ Applicable in both vadose and saturated zones

# Hydrogen Peroxide/Fenton's Reagent

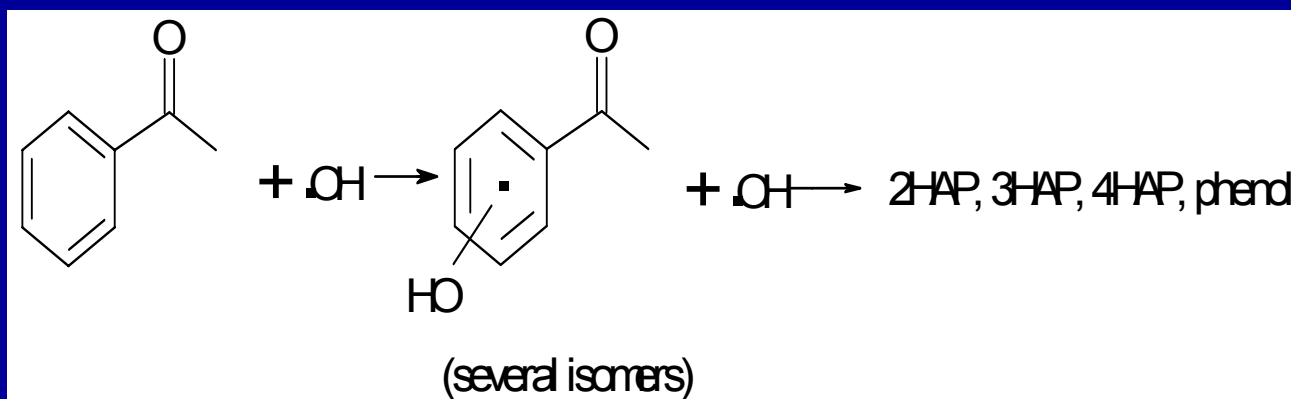
- ◆ Other heavy metals involved:  $\text{Cu}^+$ ,  $\text{VO}^{2+}$ ,  $\text{Ti}^{3+}$ ,  $\text{Cr}^{2+}$ ,  $\text{Co}^{2+}$ , and  $\text{Mn}^{2+}$
- ◆ Amendments:  $\text{Fe}^{2+}$  and acid (eg.  $\text{FeSO}_4$ )
- ◆  $\text{H}_2\text{O}_2$  stabilization may be needed ( $\text{KH}_2\text{PO}_4$ ) for safe operation and influence radius extension
- ◆ Dosage: 5-50wt%  $\text{H}_2\text{O}_2$ , multiple dosing common
- ◆ Some contaminated site has been treated by it in Alberta
- ◆ Oxidizable contaminants include:
  - Chlorinated solvents
  - Non-chlorinated solvents
  - PAH's
  - Phenols, esters, and others
  - Pesticides
  - VOC's & SVOC's
  - BTEX
  - LNAPL & DNAPL

# Hydrogen Peroxide/Fenton's Reagent

- ◆  $\text{H}_2\text{O}_2$ /Fenton reagent reaction mechanism

# Hydrogen Peroxide/Fenton's Reagent

H<sub>2</sub>O<sub>2</sub>/Fenton reagent reaction mechanism



Xu, Y. and Langford, C. H., *J. Phys. Chem. B* **1997**, 101 (16), 3115.

# Hydrogen Peroxide/Fenton's Reagent

## ◆ Advantages:

- Low chemical cost
- Relatively rapid reaction process
- Stimulation of aerobic biological activity
- Applicable over a wide range of VOC & SVOC
- Range of reliable field application information available

## ◆ Limitations:

- Safety issues from its exothermal reaction (heat and gas)
- Possible soil permeability impacted by  $\text{Fe}^{2+}$  colloid
- Temperature increase (exothermic reaction)
- Lowering of soil pH is not feasible (in situ)
- Concern of Cr(III) oxidation to Cr(VI)
- Adverse impact of Fenton's reagent on microbial populations

# Costs Comparison of Biological, Physical, and Chemical Oxidation Treatment

Treatment methods	Biological	Physical (Soil Washing)	Chemical (H <sub>2</sub> O <sub>2</sub> injection)
Contaminant	chlorinated pesticides	chlorinated pesticides	Pentachloro-phenol (PCP)
Non-capital cost (US\$/908kg)	35~1,000	50~200	30

*Richard J. Watts, matthew D. Udell, Robert M. Monsen (1993), Water Environ. Res., 65, 839*

# Objective

To understand hydrogen peroxide remediation efficiency on F3 fraction contaminated soil

# Experimental background

- ◆ Canada Wide Standard for Petroleum Hydrocarbons:
  - F1: nC6 ~ nC10
  - F2: nC10 ~ nC16
  - F3: nC16 ~ nC34
  - F4: nC34 ~ nC50
- ◆ ~60% Canada contaminated sites contain PHC
- ◆ Although this remediation technology has been tested for various contaminants in soil, most of the contaminants are volatile or semi-volatile in the range of lighter than F3 section
- ◆ Transformer oil (TO) in F3 range has not been tested



# Experimental background

## ◆ F3 fraction physical properties

- Low H/C ratio compared with F1 and F2
- Low vapor pressure ( $nC_{16}$ :  $0.008 \sim 2 \times 10^{-8}$  mmHg)
- Low Henry's law constants
- Low solubility in water ( $nC_{16}$ :  $2 \times 10^{-8}$  mg/L), hydrophobic
- Low remediation efficiencies by bioremediation
- High B. P. (b. p.:  $287 \sim 301^\circ\text{C}$ ) and  $\log K_{ow}$

## ◆ F3 fraction related contaminants

- Gas oil, residual fuel, asphalt, tar
- Engine oil, lubricant oil, and transformer oil (may contain PCBs)
- Weathered petroleum hydrocarbons

# Experimental background

- ◆ Why TO - a target contaminant?
  - Main components fall within the F3 fraction in Canada-Wide Standard for Petroleum Hydrocarbons
  - Related with PCBs contamination problem
  - Little understanding about how to treat TO contaminated soils

# Experimental Conditions

## ◆ Soil Characteristics

- Alberta New Children Hospital site clay soil, air dried
- Soil particle size < 1.25 mesh,
- Moisture content 0.56% (After air dried)
- Organic Matter 2.10%
- Iron content: 11,600 mg/kg

## ◆ TO: Voltesso N36 from Enmax (Calgary)

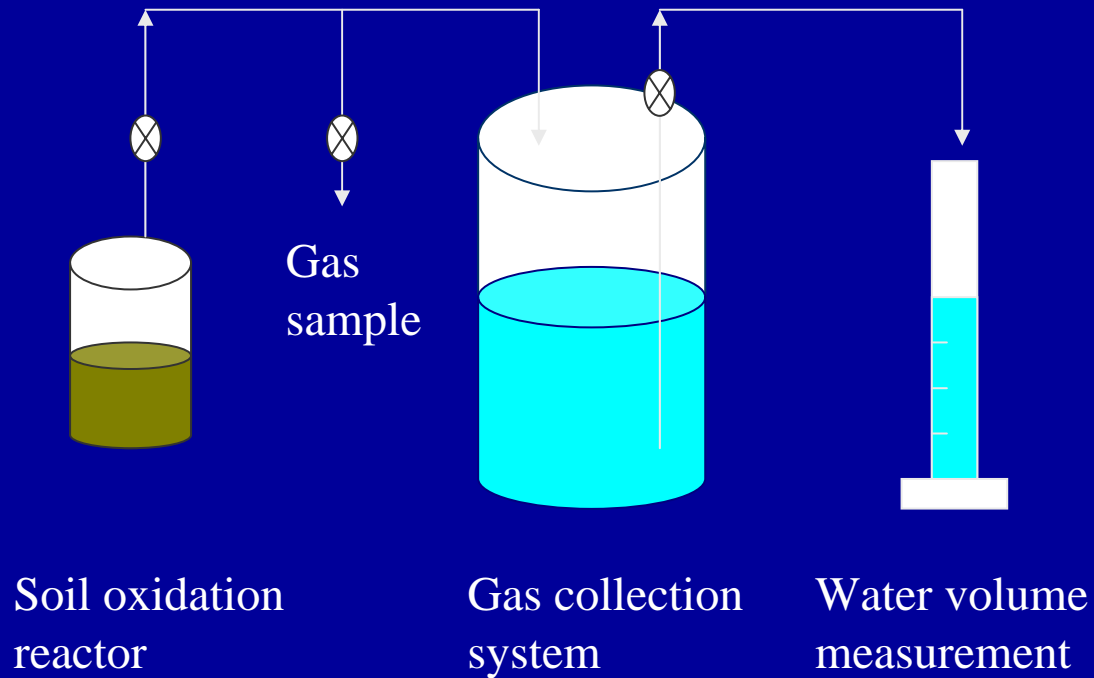
- PCBs free (<2ppm)
- Density  $d = 877 \text{ kg/m}^3$
- Good oxidation stability and insulating property
- ASTM analysis: 6% aromatic, 45% naphthenic, and 50% paraffinic hydrocarbons
- Average carbon number  $C_{27}$

## ◆ Spiked Soil

- SOM content (0~5%)
- TO content (0~5%)

# Experimental

TO contaminated soil  $H_2O_2$  oxidation test system diagram



# Results---Analytical

## ◆ Gas analysis

- Agilent GC 6890N (FID) installed with ChemStation
- Column:
  - ◆ 10 ft Haysep Q for CO<sub>2</sub>
  - ◆ 12 ft Molesieve 13X for O<sub>2</sub>, N<sub>2</sub>

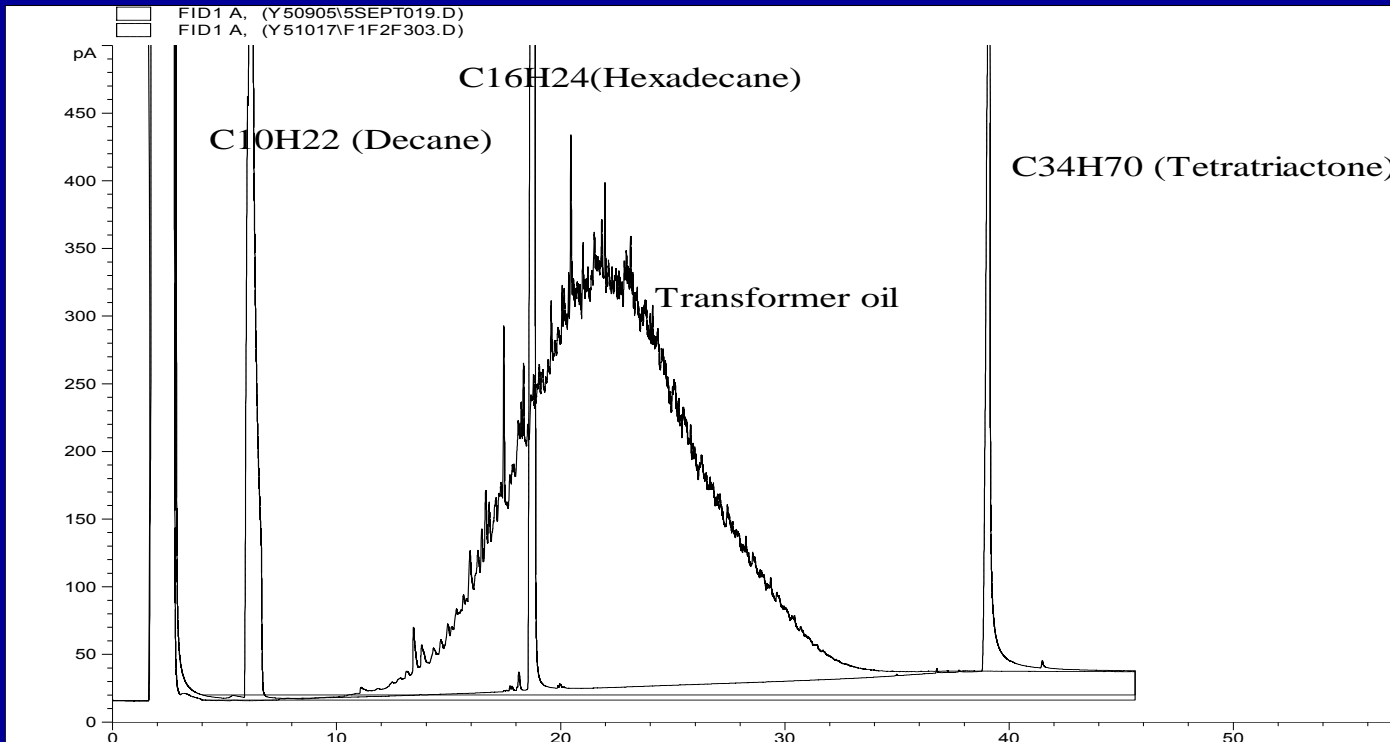
## ◆ Extracted TO analyses

- HP 6890 auto-sampler GC, FID detector
- Column HP-5(30m×0.25mm×0.25μm, ~325°C)
- ChemStation data analysis software

# Results---Analytical

Extracted TO analyses---One hump method

80°C(1minute) followed by 8°C/minute up to 325°C (10minutes)



# Results---Analytical

- ◆ Extracted TO analyses using a novel temperature profile which separates F3 fraction (three-humps method) from

F2 fraction:

Initial temperature (1minute)

30°C/minute up to 120°C (8minute) followed by

50°C/minute down to certain °C (1 minute) then

30°C/minute again up to 160°C (5minute) then

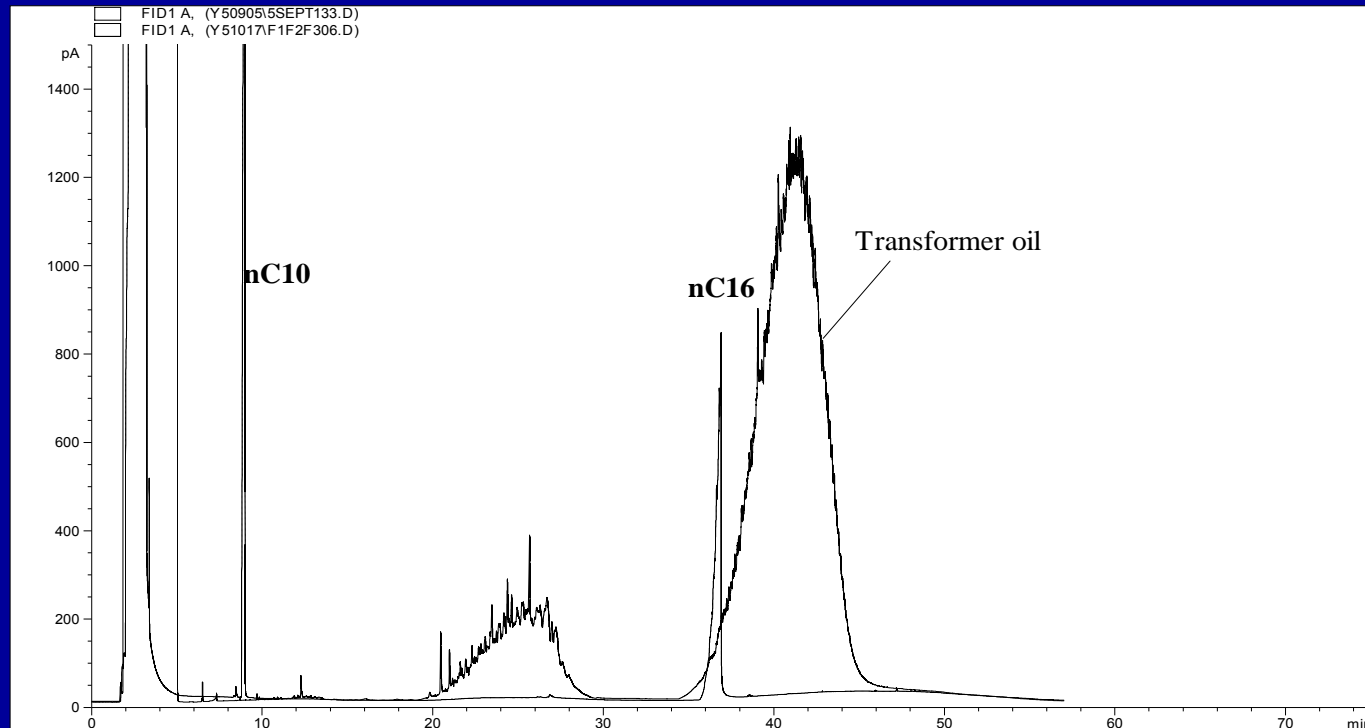
50°C/minute down to certain °C(1minute) and

30°C/minute up to 325°C (for 7minutes)

- ◆ Three humps method advantages
  - TO content can be separated into three sections
  - F2 and F3 fraction can be tested individually in the H<sub>2</sub>O<sub>2</sub> oxidation process

# Results---Analytical

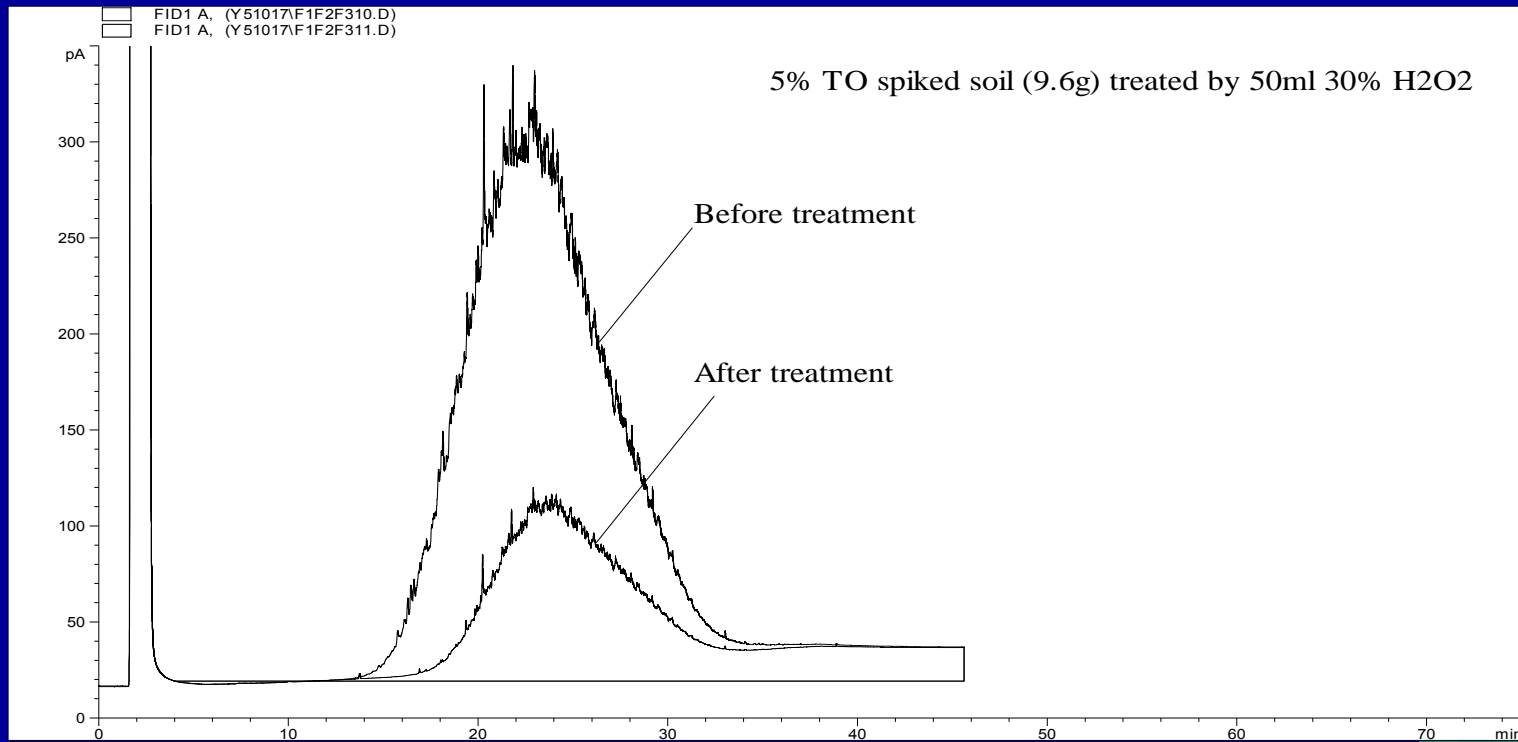
- ◆ Extracted TO analyses result (three-humps method)





# Primary experimental results

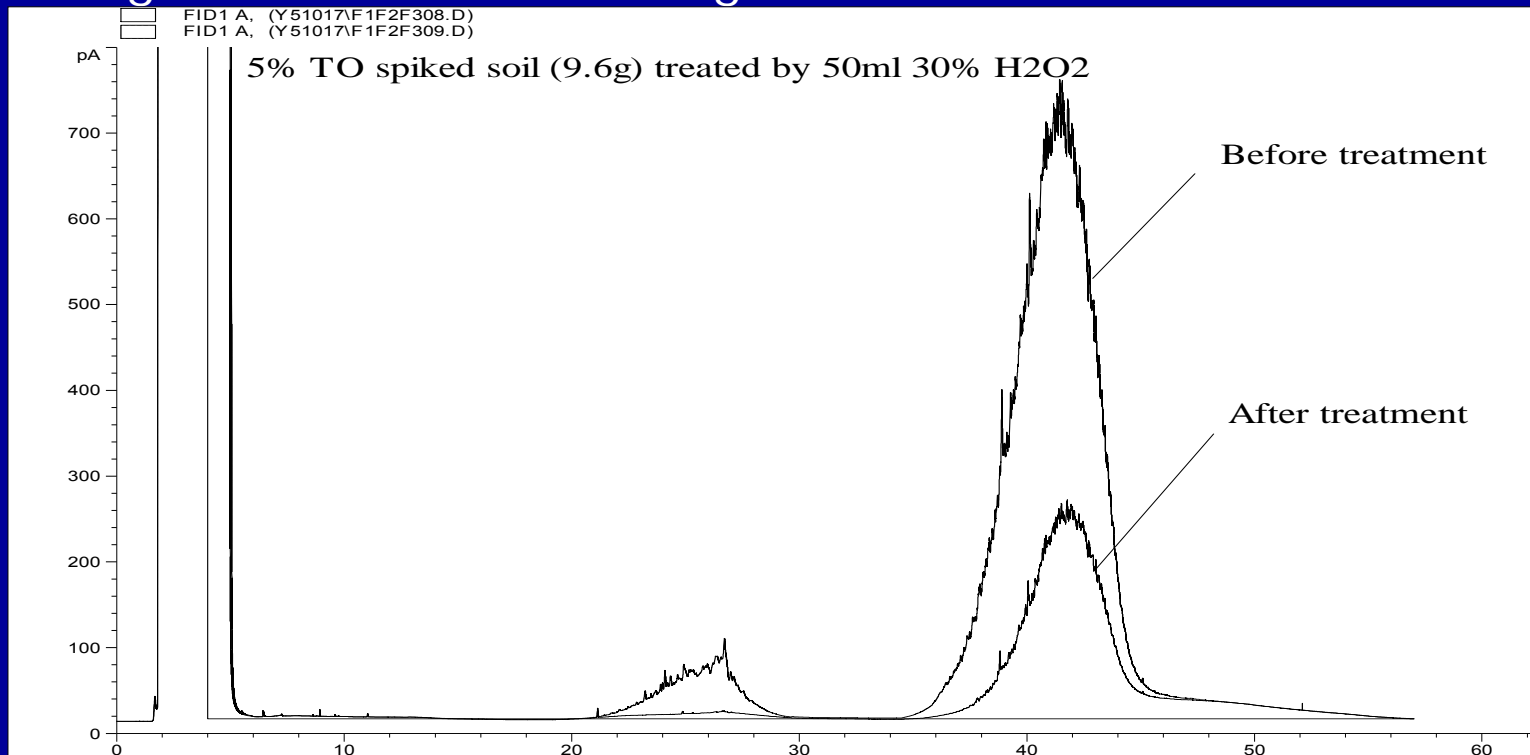
- ~10g 50,000ppm TO spiked soil + 50ml ~30% H<sub>2</sub>O<sub>2</sub> results
- Gas and heat was generated and the soil slurry was boiling for ~2 minutes during reaction



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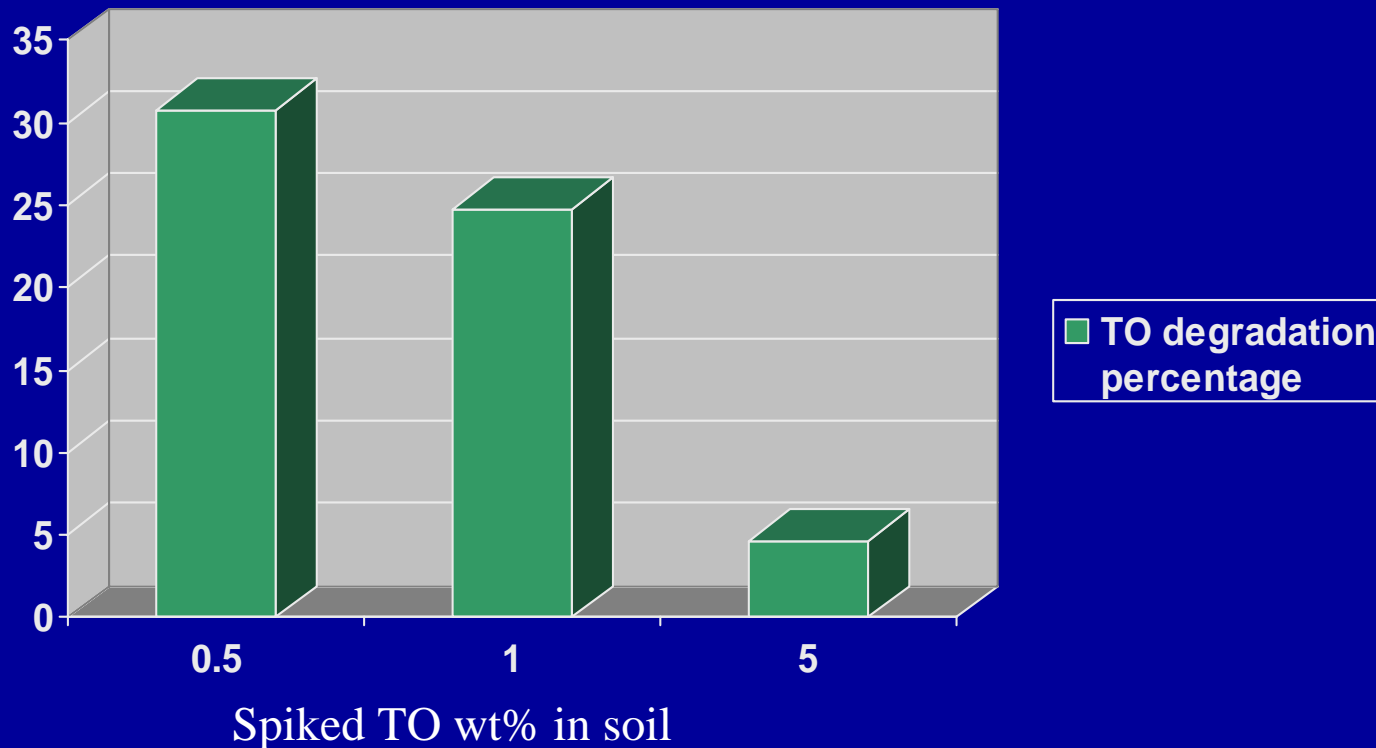
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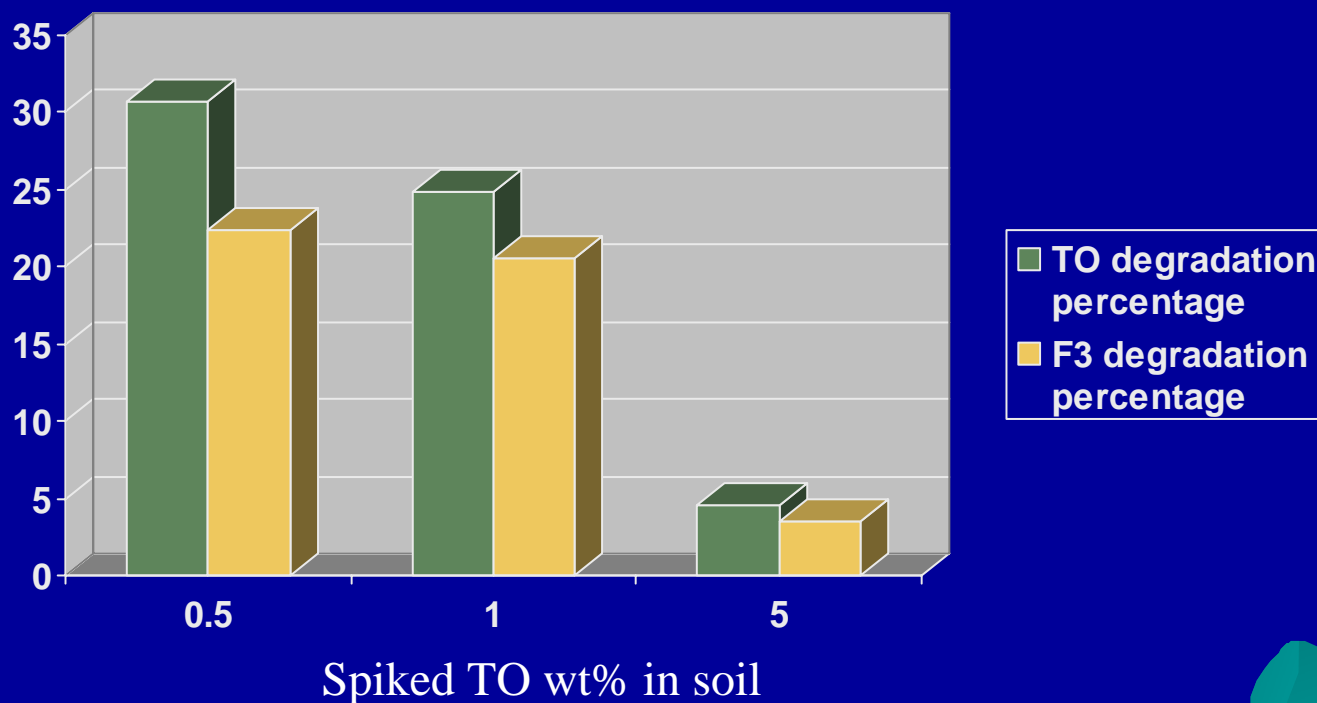
- ◆ TO degradation results(15% H<sub>2</sub>O<sub>2</sub>)
  - ~10g spiked soil (extractable SOM free, ~100ppm PCBs) + 40ml 15% H<sub>2</sub>O<sub>2</sub>



Spiked soils (TO%)	0.5	1.0	5.0
Absolute TO degradation (mg/kg soil)	880	1200	1270

# Primary experimental results

- ◆ F3 degradation results(15% H<sub>2</sub>O<sub>2</sub>)
- ◆ Experimental conditions: ~10g spiked soil (extractable SOM free, ~100ppm PCBs) + 40ml 15% H<sub>2</sub>O<sub>2</sub>



# Ongoing Work

- ◆ H<sub>2</sub>O<sub>2</sub> concentration effects
- ◆ Co-contaminant (SOM) effects
- ◆ Fe content effects
- ◆ TO containing PCBs

# Conclusions

- ◆ A soil oxidation system was set up to test evaluate  $\text{H}_2\text{O}_2$  remediation technology in laboratory
- ◆ A three-hump GC method was developed to test TO degradation in term of F3 fraction
- ◆ Primary results indicated that TO can be oxidized by  $\text{H}_2\text{O}_2$
- ◆ High  $\text{H}_2\text{O}_2$  is preferred for TO oxidation
- ◆ About 20% TO was degraded by 40 ml 15%  $\text{H}_2\text{O}_2$  for ~10g 10,000ppm spiked TO soil

Thank you!



# Questions

