

## **A CASE STUDY HOMEBUSH BAY Australia**



**Site of the  
2000 Olympic  
Games**

## **THERMAL PHASE SEPARATION (TPS)**



**An Innovative  
Volume Reduction  
Technology**

# PROCESS

## Thermal Phase Separation (TPS)

- ◆ **Thermal Phase Separation (TPS) is an indirectly heated thermal desorption technology designed for the extraction of PCBs, PAHs, pesticides, creosote, hydrocarbons, dioxins/furans, and other industrial chemicals and chlorinated contaminants from soils and sludges.**
- ◆ **Remediated material can be replaced in the excavation and the separated contaminants disposed of at a permitted facility or de-chlorinated on site.**
- ◆ **This innovative technology has successfully treated over 55,000 tonnes of hazardous waste material and has reduced the overall cost of disposal of PCB contaminated soils by up to 75%.**

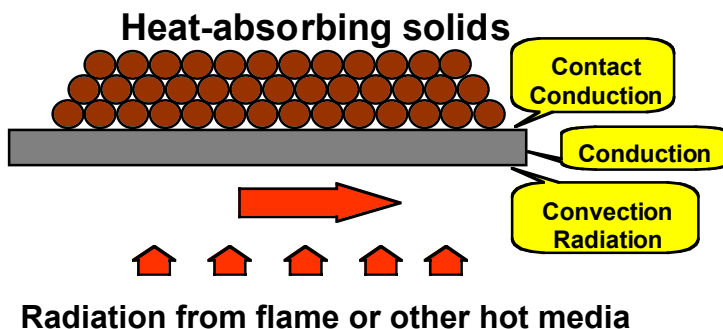
# PROCESS

## Indirect vs Direct

### INDIRECTLY HEATED

- Heat is transferred via steel plate
- Host Matrix is heated to Boiling Point
- Gases Recondensed – **NOT Incinerated**

- Lower Throughput
- PICs are not Produced
- Desorbs high BP Hydrocarbons
- Recovery & Volume Reduction



### DIRECTLY HEATED

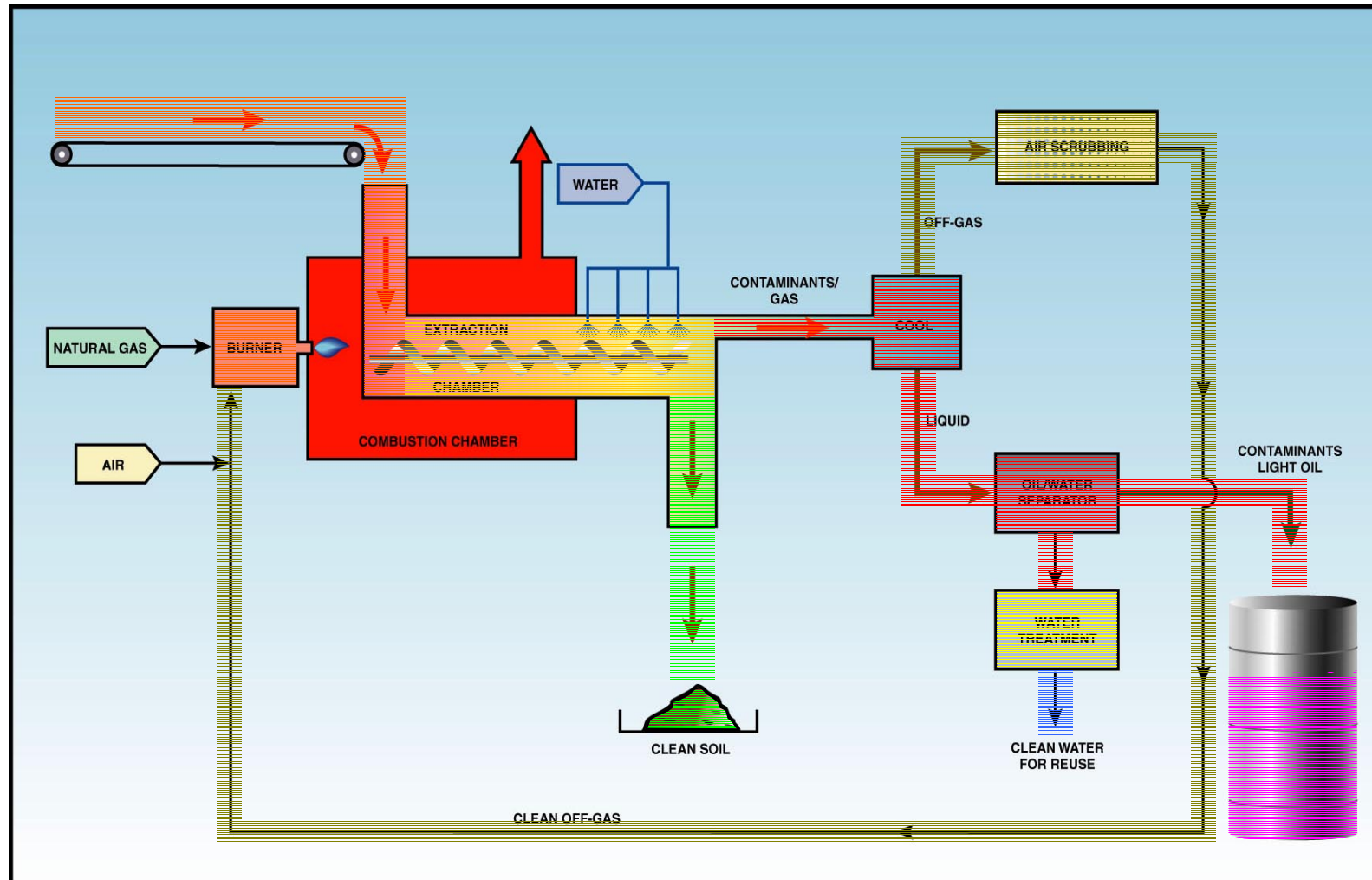
- Flame is in Contact with Contaminant
- Limitation of TPH in Feed – Dilution R'qd
- **Gases Combusted** – No Recovery

- High Throughput
- Extensive Gas Cleaning re: PICs
- Stack Emission Issues
- (6) nine DRE Requirements



# PROCESS

## Thermal Phase Separation

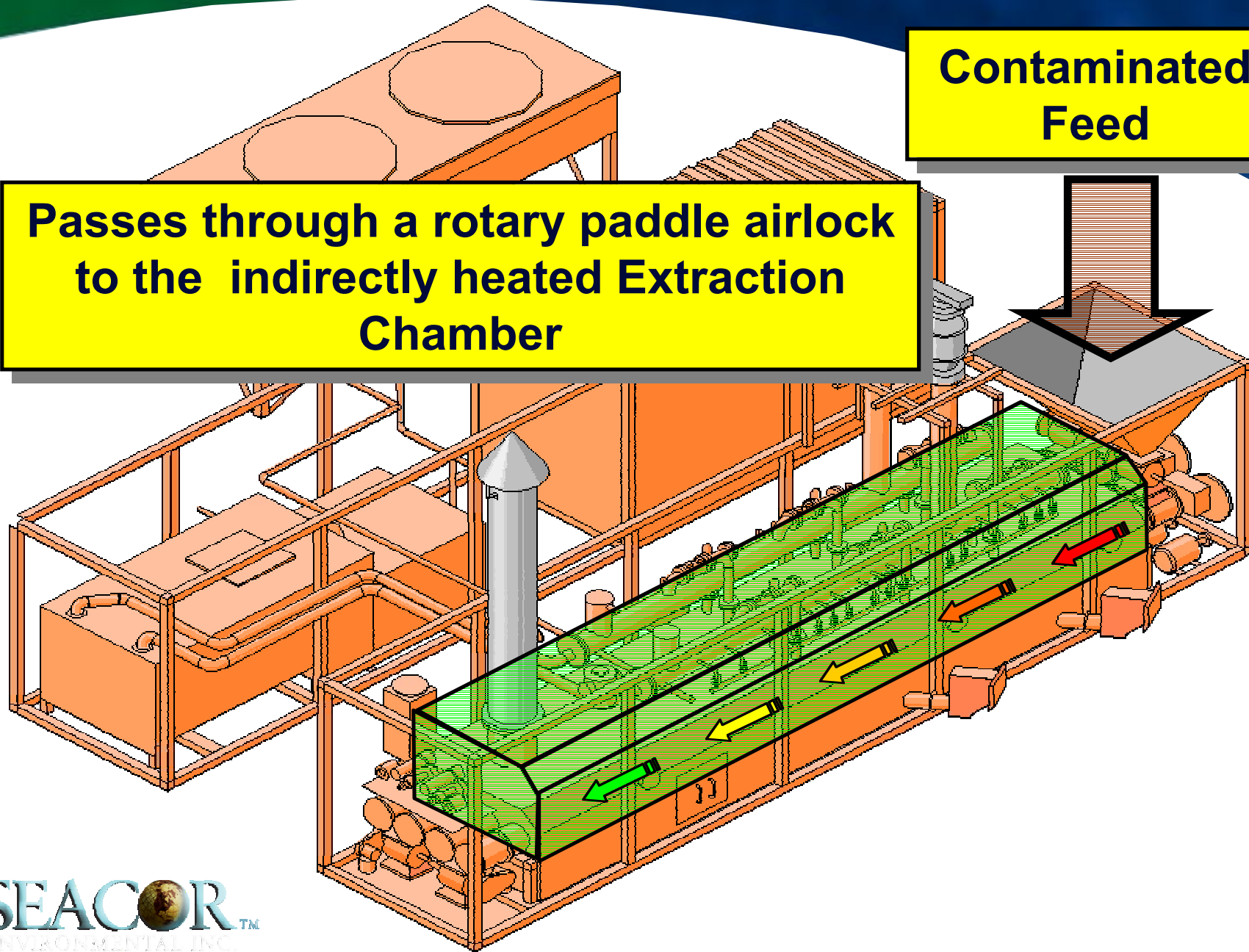


- ◆ Factors affecting performance for any thermal soil treatment processes:
  - ◆ Screening: <1-inch minus particle size
  - ◆ Moisture content: ideally <20%
  - ◆ Clay content: ideally <15%
- ◆ Over-sized material is screened & pressure washed
- ◆ Process water treated with the TPS water treatment system

# PROCESS

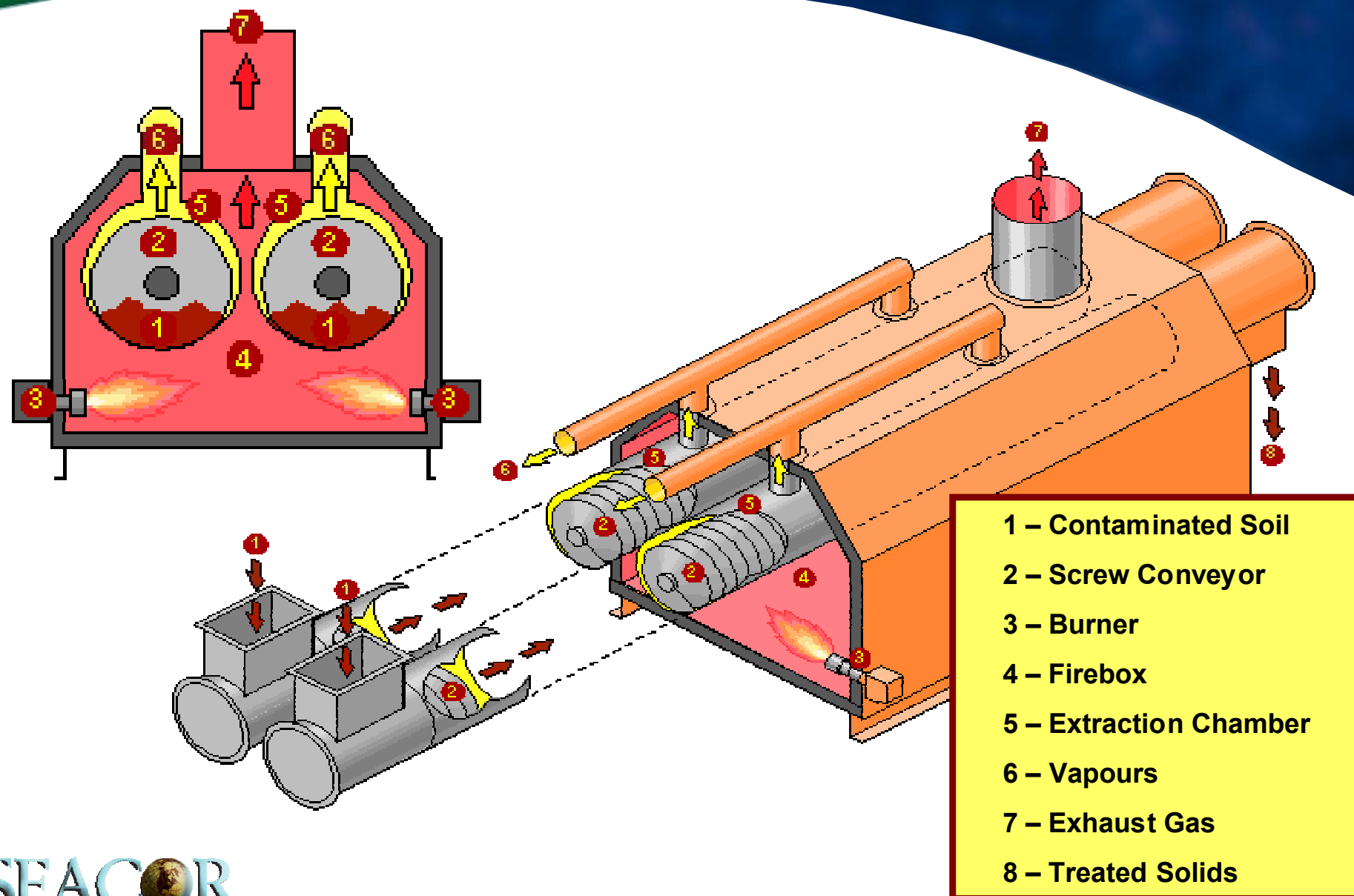
**Contaminated  
Feed**

**Passes through a rotary paddle airlock  
to the indirectly heated Extraction  
Chamber**



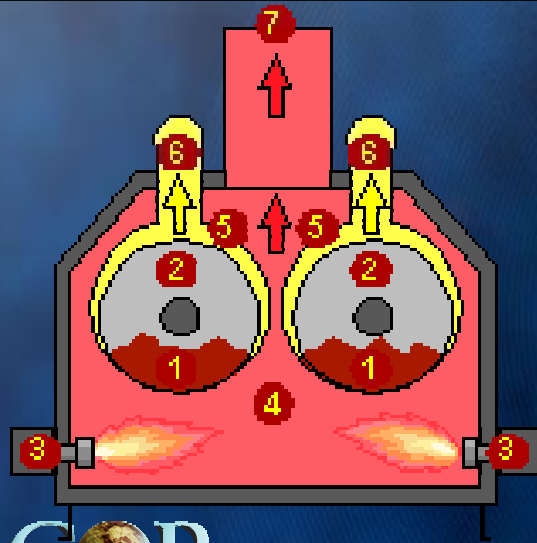
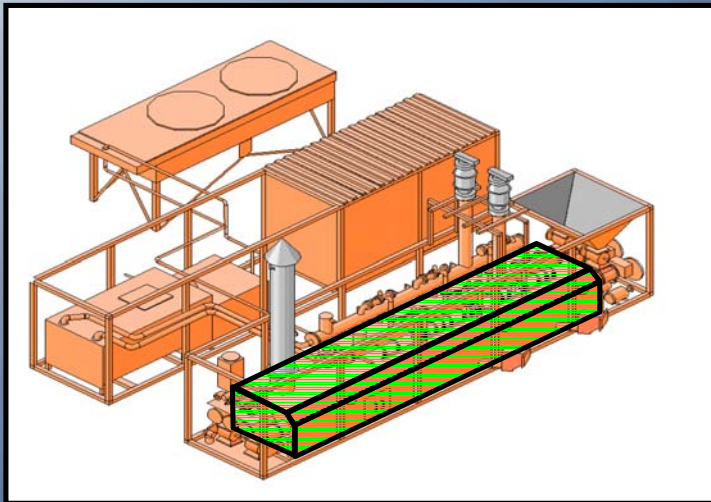
# TPS

## Internal View



# TPS

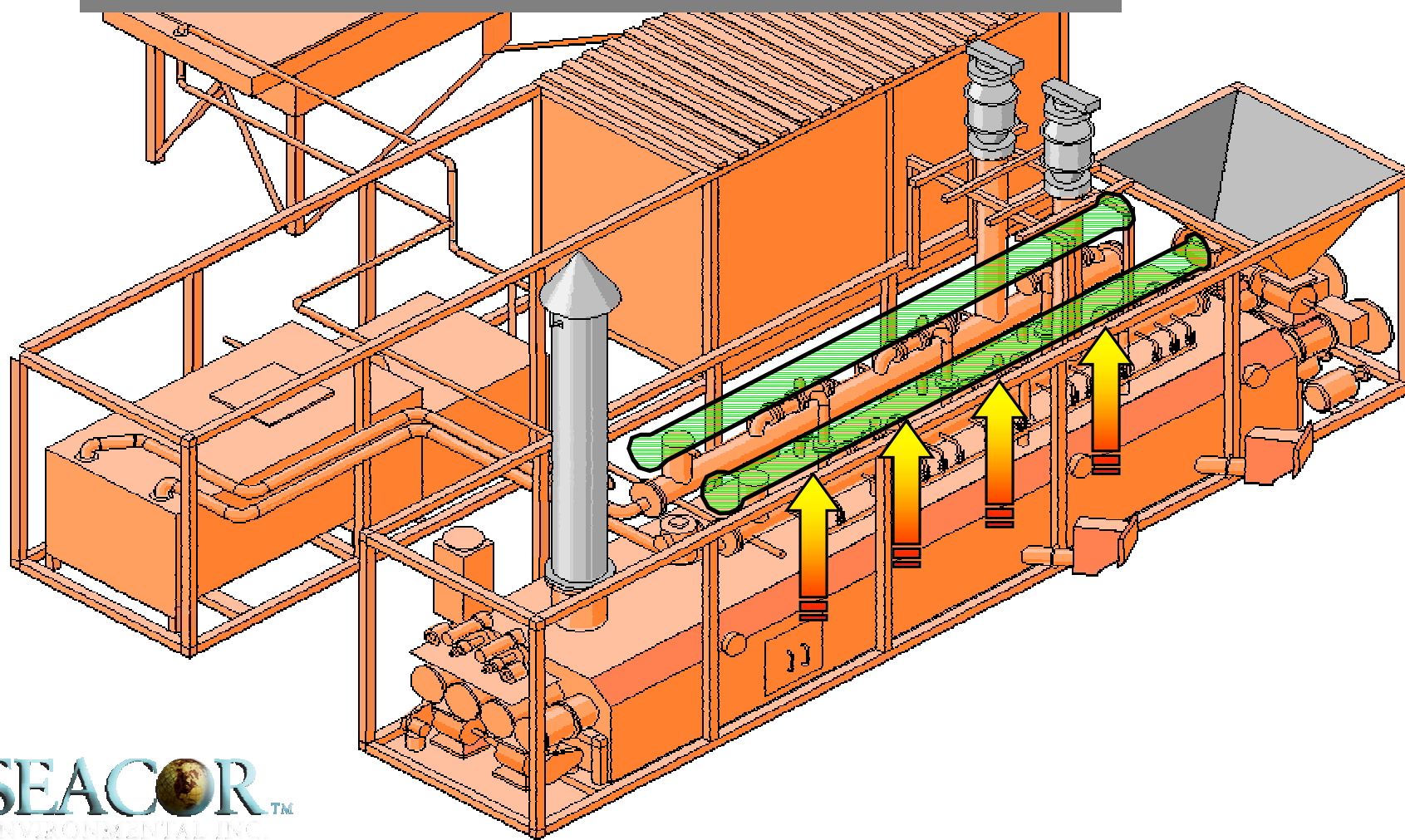
## Extraction Chamber



- ◆ Material drops through rotary airlocks
- ◆ Carried through chamber via screw augers.
- ◆ Indirectly heated using 1/2" steel.
- ◆ Extraction chamber heated with 4 MM Btu/hr burners in the fire box
- ◆ Burners fired by virgin and/or recovered diesel, propane or natural gas
- ◆ Low O<sub>2</sub> in chamber preventing combustion
- ◆ Chamber always under negative pressure preventing vapour escape.

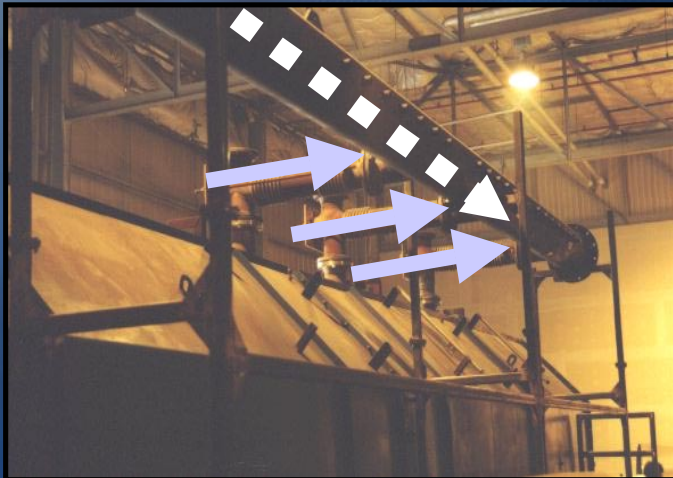
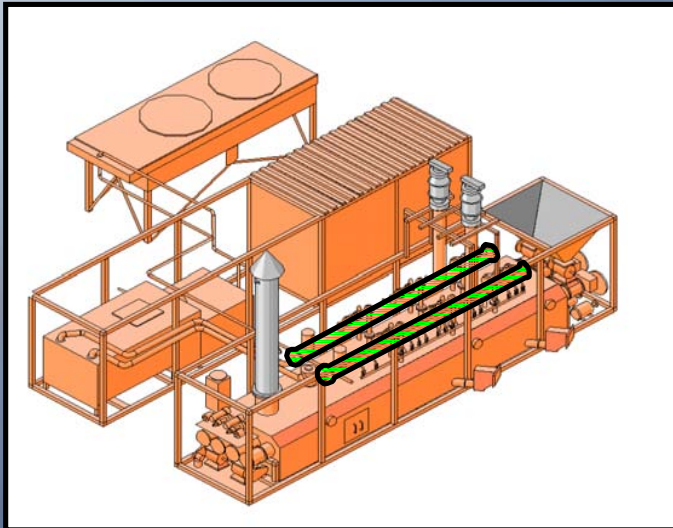
# PROCESS

**Volatilized hydrocarbons forced into  
the overhead Quench Header**



# TPS

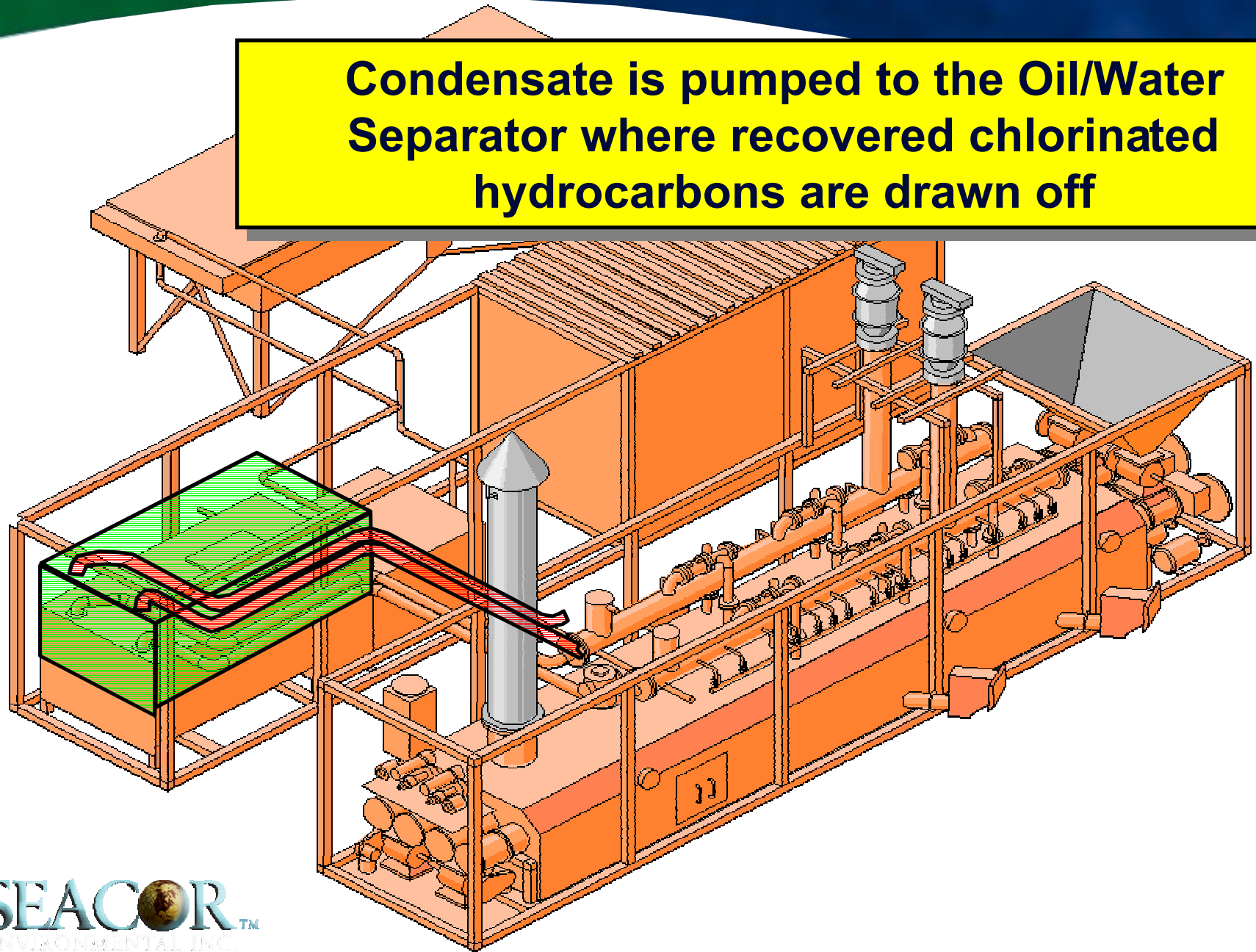
## Vapor Condensation



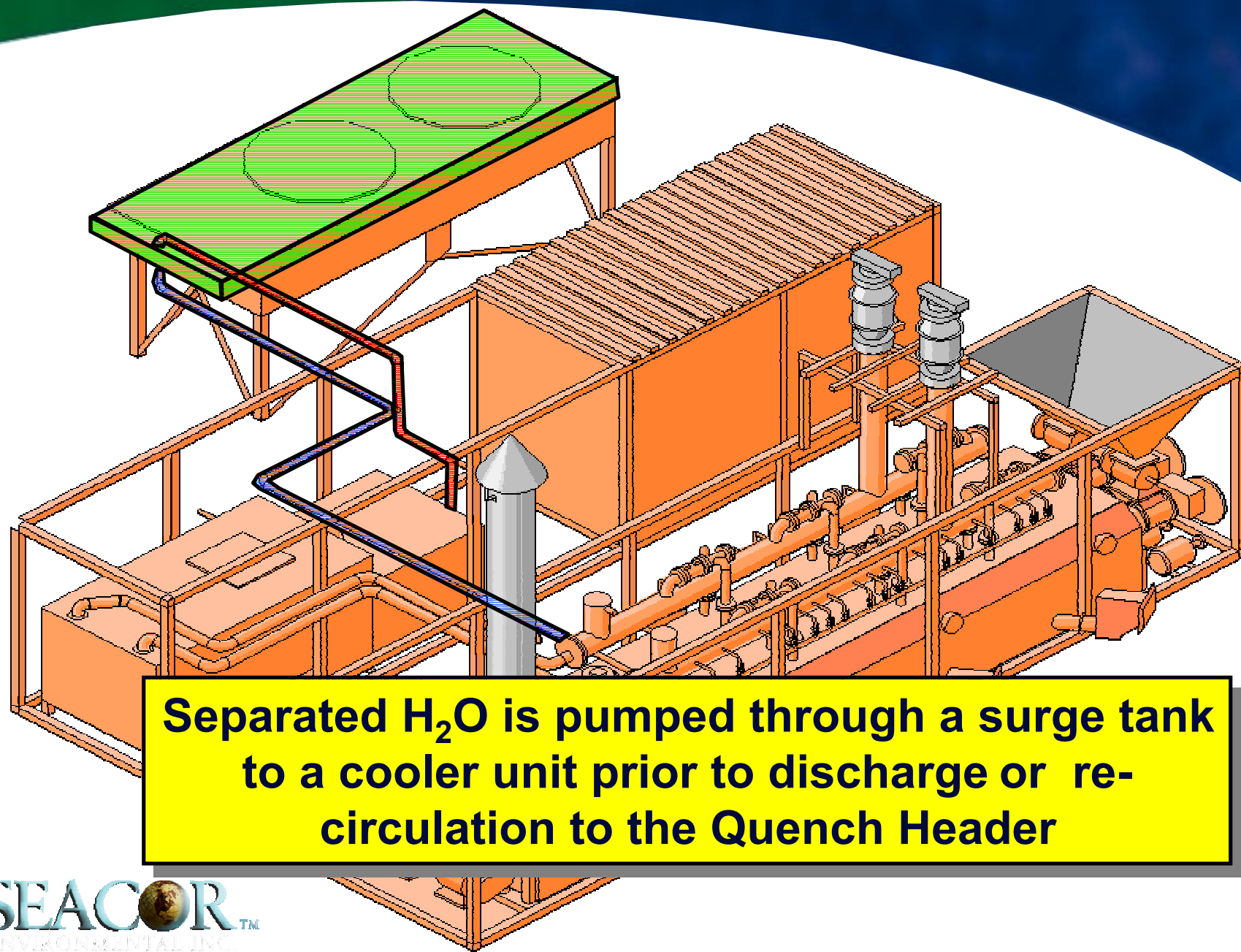
- ◆ Contaminant vapors evacuated from extraction chamber are quenched with water spray
- ◆ Contaminant liquids are dropped out and directed to an Oil/Water Separator
- ◆ Excess water vapour/steam is directed to a condenser unit and liquids are drained to an Oil/Water Separator
- ◆ Separated water is further cooled and re-circulated for quenching
- ◆ Contaminant sludge is removed from the Oil/Water separator for final destruction

# PROCESS

**Condensate is pumped to the Oil/Water Separator where recovered chlorinated hydrocarbons are drawn off**



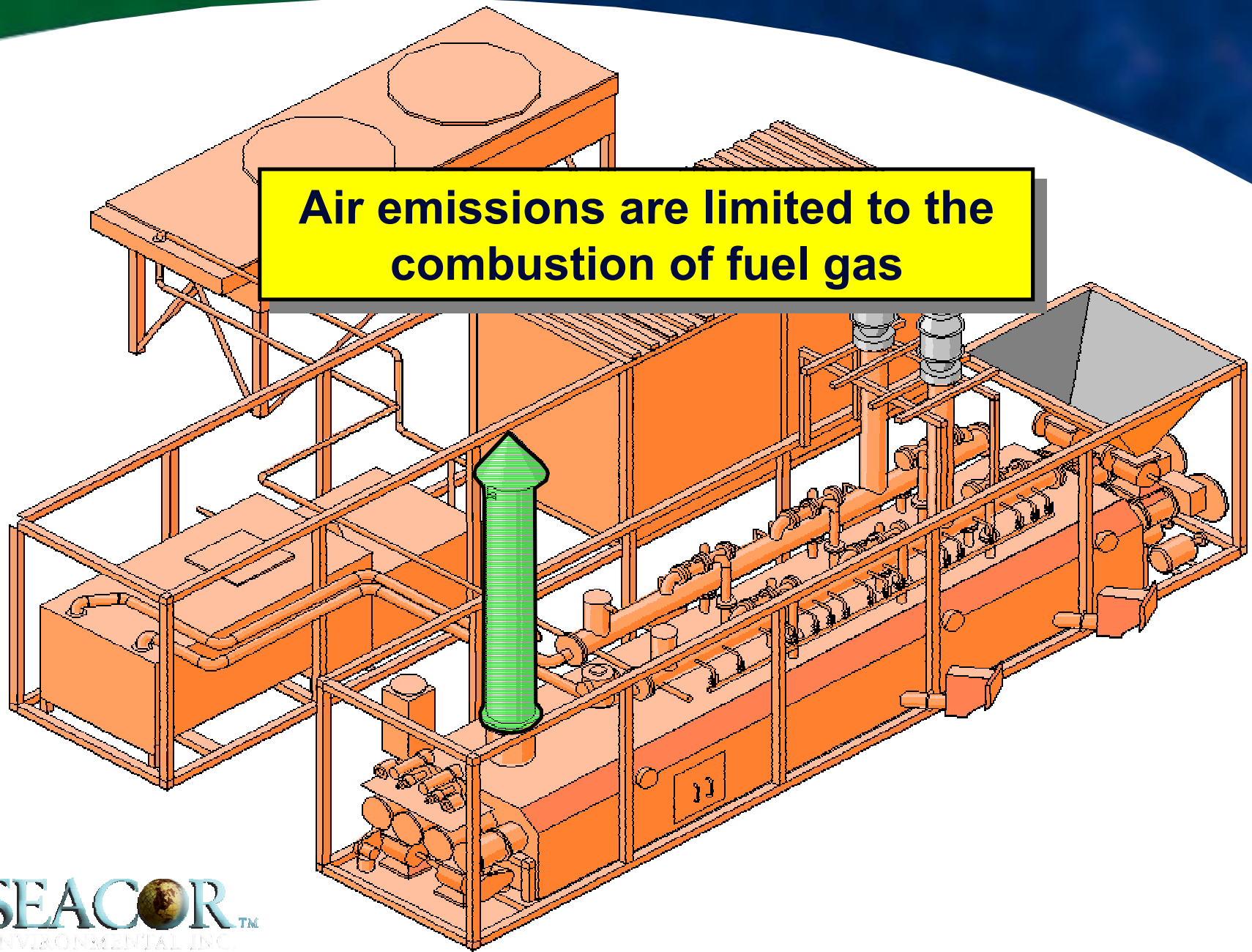
# PROCESS



**Separated H<sub>2</sub>O is pumped through a surge tank to a cooler unit prior to discharge or re-circulation to the Quench Header**

# PROCESS

**Air emissions are limited to the  
combustion of fuel gas**



# PROCESS

## Basic Process Flow

- ◆ Contaminated material is screened for the removal of foreign debris and oversized material
- ◆ Oversize material/debris is isolated for analysis and screened feedstock is fed to the TPS at the rate of ~2-3mT/hour or 55mT per day including downtime
- ◆ Treated material is removed from the TPS and placed outside of the Exclusion Zone in a quarantine pile for analysis prior to on-site internment
- ◆ Run off / Process Water is collected for analysis, treatment and either discharge, re-circulation or re-wetting
- ◆ Recovered contaminant sludge is collected, safely contained and disposed regularly

# TPS

## Treated Material Historical

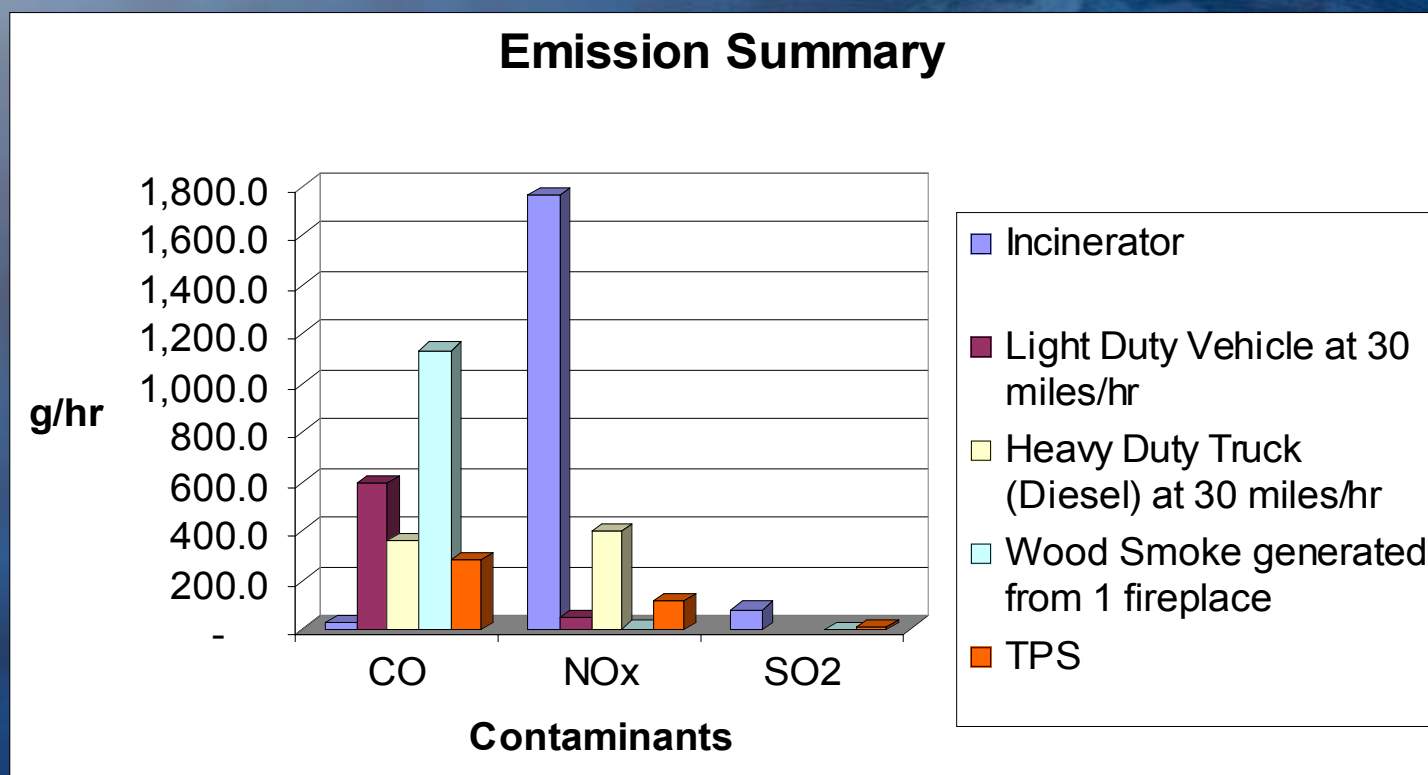
Parameter	Feed Soil (ppm)	Treated Soil (ppm)	RE (%)
Petroleum Hydrocarbons	271,000	302	99.8
Mercury	228	0.74	99.7
PAHs	6,170	21.98	99.6
Carcinogenic PAHs	377.5	9.1	97.6
Chlorophenols	1,556	3.07	99.8
PCBs 1242	521	1.71	99.67
Dioxins & Furans (TEQ) ppt	209.8	<2.7	>98.7
PCBs 1260 (Quebec)	860	1.7	99.8
PCBs 1260	169	<0.066	>99.96
PCBs 1260	5,200	6.0	99.9

# TPS

## Typical Stack Emissions

Compound	Concentration (mg/Rm <sup>3</sup> )	BC Criteria (mg/m <sup>3</sup> )	Other Provinces (mg/m <sup>3</sup> )
NOx	200	380	150-380
HCl	< 0.002	50	27-75
Particulate	14.28	20	17-20
PAH	$7.41 \times 10^{-4}$	-	0.5
CO	31.7	55	55-100
THC (as CH <sub>4</sub> )	1.83	32	32
PCB	$0.13 \times 10^{-3}$	-	0.001-0.1
Dioxins/Furans	$1.30 \times 10^{-8}$	-	$1.4 \times 10^{-7}$ - $5 \times 10^{-7}$

**Using diesel as a fuel source the TPS produces less emission than the most common uses**



## CASE STUDY

### Homebush Bay Australia

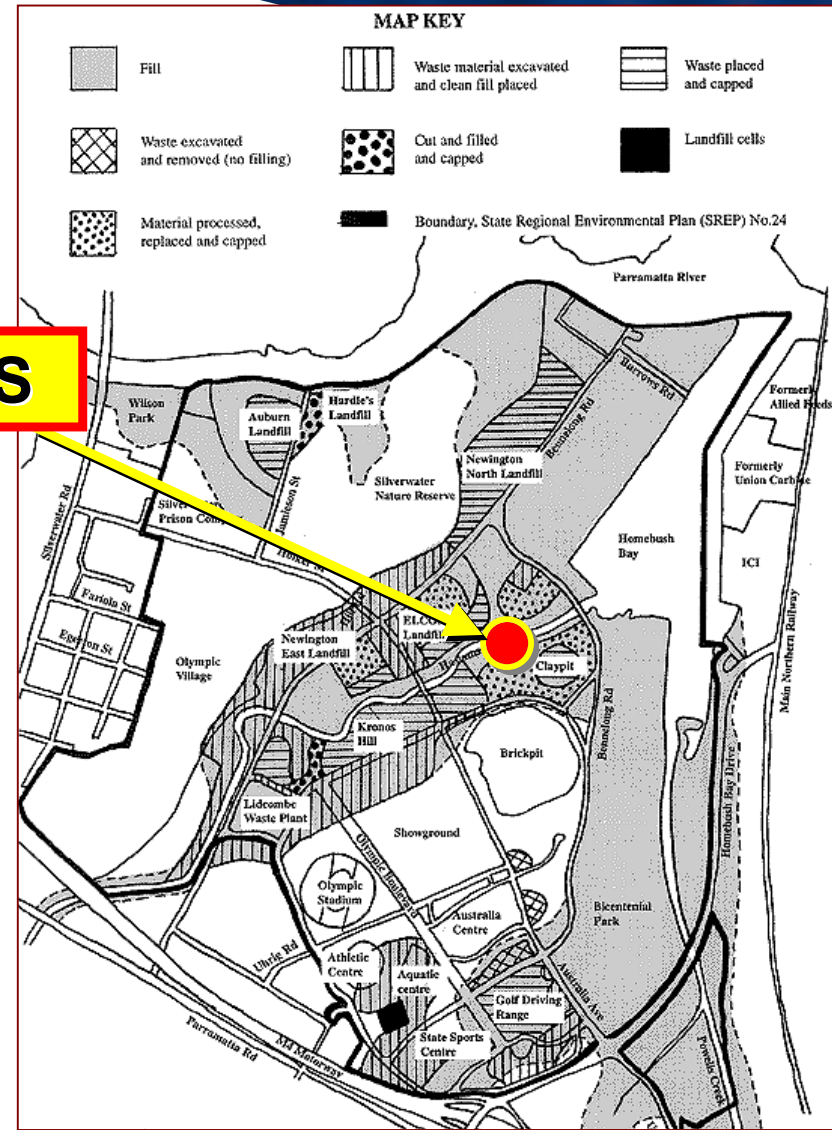
- ◆ Homebush Bay property located adjacent to the 2000 Olympic Games site in Sydney, Australia
- ◆ Former chemical manufacturing landfill site including chlorbenzene, chlorophenol, dioxin/furan and Agent Orange
- ◆ OCA declared 2000 Olympics to be the Green Games and pledges clean up prior to the games
- ◆ Australian Defense Industries (ADI) selects TPS as the only technology worldwide that can achieve the remediation goals safely

# CASE STUDY

## Homebush Bay Australia

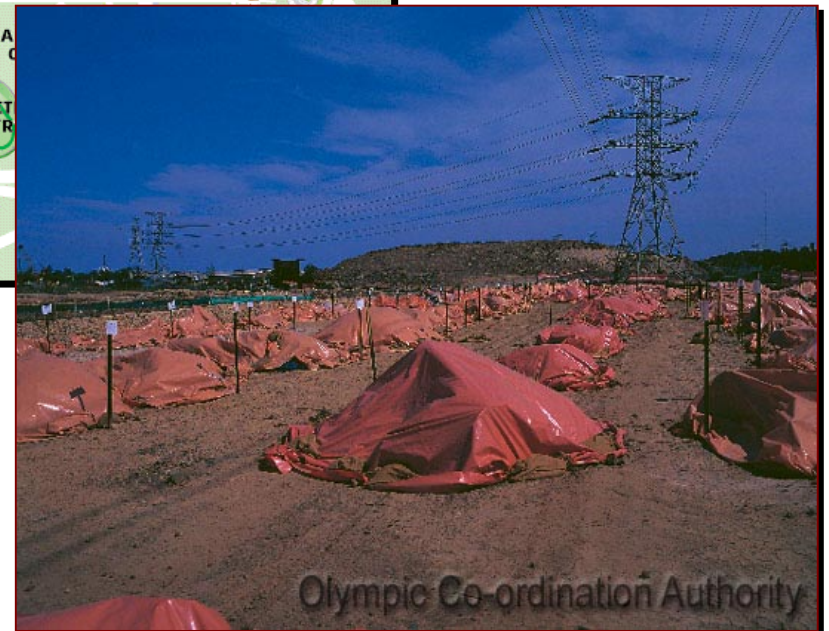
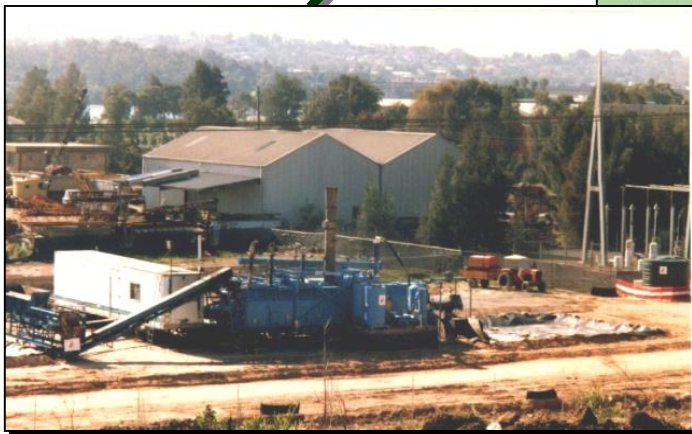


TPS



# CASE STUDY

## Homebush Bay Australia



# CASE STUDY

## Homebush Bay Australia

<b>Contaminant</b>	<b>Feed</b>	<b>Criteria</b>	<b>Result</b>
<b>Soil Treatment</b>			
<b>Dioxin/Furan</b>	283 ppb	<10 ppb	0.075 ppb
<b>Schedule Chemical Waste*</b>	4,603 ppm	<1 ppm	0.28 ppm
<b>Air Emissions**</b>			
		mg/Nm <sup>3</sup>	mg/Nm <sup>3</sup>
<b>Particulates (as TSP)</b>		100	1.8
<b>NO<sub>x</sub> as NO<sub>2</sub></b>		1200	70.8
<b>CO</b>		55,000	20.8
<b>PAHs</b>		190	0.0016
<b>SO<sub>3</sub> as H<sub>2</sub>SO<sub>4</sub> mist (as H<sub>2</sub>SO<sub>4</sub>)</b>		90	0.64
<b>Heavy metal (aggregate)</b>		5.0	.41
<b>Benzene</b>		270	<0.4
<b>Mono-chlorobenzene</b>		540	<0.4
<b>1,2-Dichlorobenzene</b>		27,000	<0.4
<b>Pentachlorophenol</b>		46	<0.00002
<b>Phenol</b>		98	0.214
<b>Dioxin/Furan (I-TEQ***)</b>	-----	<0.1 ng/Nm <sup>3</sup>	0.045ng/Nm <sup>3</sup>

\* Schedule Chemical Waste – primary compounds: chlorobenzenes & chlorophenols

\*\* Average of 5 independent stack tests conducted using US EPA standard

\*\*\* International Toxicity Equivalency Quotient

# CASE STUDY

## Homebush Bay Australia

### STACK GAS MONITORING FROM ITD PLANT

Gas Sample Sampling Date				Day 2 19-Sep-99	Day 3 20-Sep-99	Day 5 22-Sep-99	Day 11 28-Sep-99	Day 15 2-Oct-99
Analyte being Monitored	Units	Limit of Detection	Licence Criteria					
Chlorine	mg/Nm <sup>3</sup>	0.05	200	nd	nd	nd	0.10	nd
Hydrochloric Acid	mg/Nm <sup>3</sup>	0.03	100	nd	nd	nd	0.24	nd
Particulates (Dust)	mg/Nm <sup>3</sup>	1	100	4	2	nd	nd	nd
NO <sub>x</sub> (as NO <sub>2</sub> )	mg/Nm <sup>3</sup>	1	1200	82	66	68	66	72
Carbon Monoxide	mg/Nm <sup>3</sup>	1	55000	14	38	28	14	10
Dioxins (I-TEQ) *	mg/Nm <sup>3</sup>	0.001 x 10 <sup>-7</sup>	1.0 x 10 <sup>-7</sup>	0.515 x 10 <sup>-7</sup>	1.51 x 10 <sup>-7</sup>	0.101 x 10 <sup>-7</sup>	nd	0.091 x 10 <sup>-7</sup>
PAH's	mg/Nm <sup>3</sup>	0.0006	190	0.0018	0.0040	nd	0.0010	nd
H <sub>2</sub> SO <sub>4</sub> (as SO <sub>3</sub> )	mg/Nm <sup>3</sup>	0.04	90	0.23	0.41	2.00	0.33	0.25
Heavy metal (aggregate)	mg/Nm <sup>3</sup>	0.0005	5	0.29	0.66	0.36	0.37	0.39
Cd or Hg (as organic Hg)	mg/Nm <sup>3</sup>	0.0005	0.82	0.0027	0.0005	nd	0.0008	0.0014
Benzene	mg/Nm <sup>3</sup>	0.4	270	nd	nd	nd	nd	nd
Total Chlorobenzenes	mg/Nm <sup>3</sup>	0.4	540	nd	nd	nd	nd	nd
1,2-Dichlorobenzene	mg/Nm <sup>3</sup>	0.4	27000	nd	nd	nd	nd	nd
Pentachlorophenol	mg/Nm <sup>3</sup>	0.00002	46	nd	nd	nd	nd	nd
Phenol	mg/Nm <sup>3</sup>	0.04	98	0.34	0.61	nd	nd	nd

# RECOGNITION

## Homebush Bay Australia

### **Greenpeace Congratulates OCA As Treatment Of Toxic Waste At Olympic Site Begins**

**Sydney Wednesday 11 August, 1999:** Greenpeace today congratulated the Olympic Coordination Authority (OCA) for cleaning up 400 tonnes of dioxin contaminated waste at the Olympic site.

"As we approach 400 days until the Sydney Olympics, Greenpeace believes this clean-up will be an important legacy of the Green Games and a showcase for world-class technology," said Greenpeace toxic pollution campaigner Dr Darryl Luscombe. "The OCA is to be congratulated for choosing to destroy this dioxin contaminated waste in a way that minimises the impacts on the environment."

The system\* chosen by the OCA and implemented by Australian Defense Industries (ADI)\*\* does not use incineration to destroy the dioxins. Instead it breaks down the chemical products to their constituent parts, making them safer. If operated to high standards, Greenpeace believes this type of technology is much better for the environment than incineration or putting it in landfill.

"The OCA has chosen to treat this waste in a manner that is an example to the rest of the world," said Dr Luscombe.

\*The Thermal Phase Separation technology

\*\*SCC Environmental's Australian partner

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## **THERMAL PHASE SEPARATION (TPS)**



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## PROJECT BRIEF

SHERBROOKE

**Client:** Various

**Tonnage:** 1,000mT

**Equipment Designation:** TPS-1

**Operations Commenced:** June 1997

**Operations Completed:** October 1998

**Feed Contaminant:** PCB, PAH, TPH

**Average Treated Solids:** Below Criteria



## PROJECT BRIEF

## WESTFIELD

**Client:** Westfield, Victoria, Australia

**Tonnage:** 700mT

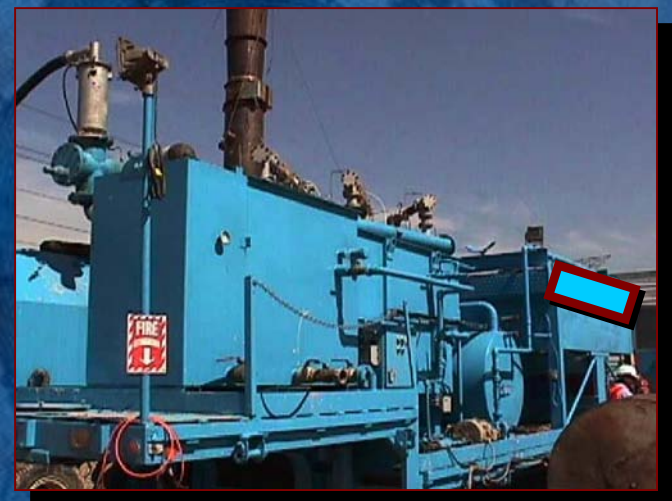
**Equipment Designation:** TPS-1

**Operations Commenced:** January 2000

**Operations Completed:** February 2000

**Feed Contaminant:** PCB

**Avg. Treated Solids:** <1ppm



# PROJECT BRIEF

## ARGENTINA

**Client:** Argentina

**Tonnage:** 5,100 tons

**Equipment Designation:** TPS-1V3

**Operations Commenced:** January 2001

**Operations Completed:** October 2001

**Feed Concentrations (by volume):**

22% hydrocarbon

26% water

52% solids

**Average Treated Solids:** <0.1% TPH

**Base Oil:** Diesel – reused as fuel



# PROJECT BRIEF

## ECUADOR

**Client:** ARCO/AGIP

**Remote helicopter site in Amazon rainforest**

**Tonnage:** 13,000 tons

**Equipment Designation:** TPS-2

**Operations Commenced:** April 1999

**Operations Completed:** May 2000

**Feed (v/v):** 20% hydrocarbon

25% water

55% solids

**Average Treated Solids:** <.5% TPH

**Base Oil:** Linear Paraffin. Recycled as base oil

**Total environmental compliance plus  
>\$1.0 million in recovered base oil.**



## PROJECT BRIEF

**BOLIVIA**

**Client:** Major Oil Company in Bolivia

**Tonnage:** 25,000 tons (to date)

**Equipment Designation:** TPS-2

**Operations Commenced:** December 2000

**Operations Completed:** continues to end of 2002

**Feed(v/v)**      23% hydrocarbon

22% water

55% solids

**Avg Treated Solids:** <0.5% TPH

**Base Oil:** Diesel reused as fuel



## PROJECT BRIEF

## KAZAKHSTAN

**Client:** Major Oil Company

**Tonnage:** 20,000 tons (to date)

**Equipment Designation:** TPS-2

**Operations Commenced:** June 2000

**Operations Completed:** 2003

**Feed(v/v)** 20% hydrocarbon

15% water

65% solids

**Avg. Treated Solids:** <0.5% TPH

**Base Oil:** Diesel recycled as base oil



# TPS

## Proven Technology

**TPS Technology is Readily Recognizable  
in Canada and around the world**



- ◆ **Permitted in most jurisdictions including Ontario and Quebec (1998)**
- ◆ **Completed a Commercial Demonstration in Quebec (1997-98)**
- ◆ **Completed Federal ETV Certification (1998)**
- ◆ **Completed DESRT (similar to US EPA SITE) Testing (1995)**

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